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Gas flow mechanisms in fractured low permeability reservoirs.

OGOUN, E., AISUENI, F., OGUNLUDE, P. and GOBINA, E.

2021



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CONTENT OUTLINE

- 1. Introduction/overview
- 2. Aim
- 3. Materials and methods
- 4. Data summary
- 5. Results and discussion
- 6. Conclusion
- 7. Questions





INTRODUCTION/OVERVIEW

1. Gas demand and production has enhanced the diversification of economic activities from oil, with United State of America, China and Middle East in full swing unconventional gas revolution.



Gas consumption

Gas production growth by region



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INTRODUCTION/OVERVIEW

- Unconventional gas reservoirs usually have very low matrix permeability, less than 0.1mD and a matrix porosity of less than 10%.
- 2. Unconventional reservoirs in most cases require hydraulic fracturing/fracking to liberate gas at economical quantity to the wellbore.
- 3. The reservoirs produce at a low flow rate under radial flow conditions without hydraulic fracturing, but after a successful fracture treatment the mechanism of the gas flow in the formation changes from radial flow to linear flow.



RESEARCH AIM

 This research is designed to experimentally study the factors that influence the gas flow mechanism in low permeability reservoir.





MATERIALS AND METHODS

- (1) pressure gauge
- (2) pressure valve
- (3) gas regulator
- (4) gas cylinder
- (5) thermometer
- (6) thermocouple transducer
- (7) flow meter
- (8) heat regulator
- (9) heat jacket and
- (10) core holder.





MATERIALS AND METHODS



Experimental set-up



DATA SUMMARY

	A	в	с	D	E	F	G	н	I	L	к
1	OXYGEN (O2) GAS : 15NM AT ROOM TEMPERATURE (20 DEGREE CELCIUS)										
	Inlet	Outlet	Inlet	Outlet	Pressure	Average	Core	Flowrate	Flowrate	Flux	Permeance
2	pressure	pressure	pressure	pressure	drop (Pa)	Pressure	Surface	(LPM)	(M ³ /S)	(M ³ /M ² S)	(M ³ /M ² SPa)
2	(Bar) 1 2	(Bar) 1	(Pa) 120000	(Pa) 100000	20000	(Pa) 110000	Area (M ⁻) 5 3 3 9	0.378	2 521E-05	4 722F-06	2 361F-10
4	1.2	1	160000	100000	60000	130000	5 3 3 9	1 478	9.854F-05	1.846F-05	3.076F-10
5	2	1	200000	100000	100000	150000	5 3 3 9	2 578	0.0001719	3.219F-05	3.219F-10
6	2.4	1	240000	100000	140000	170000	5.339	3.678	0.0002452	4.593E-05	3.28E-10
7	2.8	1	280000	100000	180000	190000	5.339	4.778	0.0003185	5.966E-05	3.315E-10
8	3.2	1	320000	100000	220000	210000	5.339	5.878	0.0003919	7.34E-05	3.336E-10
9	3.6	1	360000	100000	260000	230000	5.339	6.978	0.0004652	8.713E-05	3.351E-10
10	4	1	400000	100000	300000	250000	5.339	8.078	0.0005385	0.0001009	3.362E-10
11											
12			CARBON DIC	DXIDE (CO2)	GAS : 15NN	Ι ΑΤ ROOM	TEMPERATU	JRE (20 DEG	REE CELCIUS)	
	Inlet	Outlet	Inlet	Outlet	D	Average	Core	El averat a	Flowmate	Elux	Do rm o on co
	pressure	pressure	pressure	pressure	Pressure	Pressure	Surface	Flowrate	riowrate	riux	permeance
13	(Bar)	(Bar)	(Pa)	(Pa)	urop (Fa)	(Pa)	Area (M ²)		(IMF7S)	(101-7101-5)	(M ⁻ /M ⁻ SPa)
14	1.2	1	120000	100000	20000	110000	5.339	0.805	5.367E-05	1.005E-05	5.026E-10
15	1.6	1	160000	100000	60000	130000	5.339	1.805	0.0001203	2.254E-05	3.756E-10
16	2	1	200000	100000	100000	150000	5.339	2.805	0.000187	3.503E-05	3.503E-10
17	2.4	1	240000	100000	140000	170000	5.339	3.805	0.0002537	4.751E-05	3.394E-10
18	2.8	1	280000	100000	180000	190000	5.339	4.805	0.0003203	6E-05	3.333E-10
19	3.2	1	320000	100000	220000	210000	5.339	5.805	0.000387	7.249E-05	3.295E-10
20	3.6	1	360000	100000	260000	230000	5.339	6.805	0.0004537	8.497E-05	3.268E-10
21	4	1	400000	100000	300000	250000	5.339	7.805	0.0005203	9.746E-05	3.249E-10
22											
23		AIR : 15NM AT ROOM TEMPERATURE (20 DEGREE CELCIUS)									
	Inlet	Outlet	Inlet	Outlet	Pressure	Average	Core	Flowrate	Flowrate	Flux	Permeance
24	pressure	pressure	pressure	pressure	drop (Pa)	Pressure	Surface	(LPM)	(M^{3}/S)	(M^3/M^2S)	(M^3/M^2SPa)
24	<u>(Bar)</u>	(Bar)	(Pa)	(Pa)	20000	(Pa)	Area (M ²)	0 752		0.2015.06	4 6065 10
25	1.2	1	120000	100000	20000	120000	5.339	0.752	0.0001168	9.391E-06	4.696E-10
20	1.6	1	200000	100000	100000	150000	5.339	1.752	0.0001188	2.1000-05	3.646E-10
27	2	1	200000	100000	140000	170000	5.339	2.752	0.0001835	4.6855.05	3.437E-10
20	2.4	1	240000	100000	180000	190000	5.339	3.752 4 752	0.0002301	5 934E-05	3.347E-10
30	2.8	1	320000	100000	220000	210000	5.339	5 752	0.0003835	7 1835-05	3.257E-10
31	3.2	1	360000	100000	260000	230000	5 3 3 9	6 752	0.0004502	8 431F-05	3.243E-10
32	<u>3.0</u>	1	400000	100000	300000	250000	5 2 2 9	7 752	0.0005168	9.68F-05	3 227F-10
32	4		400000	100000	300000	230000	5.339	/./52	0.0003168	9.08E-05	3.2272-10

RESULTS/DISCUSSION

• EFFECT OF PRESSURE DROP ON FLUX FOR THE DIFFERENT GASES AT ROOM TEMPERATURE.

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Effect of pressure drop on flux for the different gases at room temperature

RESULTS/DISCUSSION

• EFFECT OF AVERAGE PRESSURE ON PERMEANCE FOR THE DIFFERENT GASES AT ROOM TEMPERATURE

Effect of average pressure on permeance for the different gas at room temperature

RESULTS/DISCUSSION

EFFECT OF PRESSURE DROP ON FLUX FOR THE DIFFERENT GASES AT ROOM TEMPERATURE AT DARCY'S REGION

In Darcy flow the proportionality constant κ, is called the Darcy permeability, and is used to characterize the porous medium. Thus, the Darcy formula for linear displacement is given by equation

 $q/A = Q = -\kappa \Delta P/\mu \delta$

The flux Q was plotted against the pressure drop ΔP with the slop of the graph equals $-\kappa/\mu\delta$

CONCLUSION

- 1. The matrix permeability of unconventional gas reservoir is usually very low, less than 0.1 milli Darcy and requires fracture treatment for effective productivity.
- 2. The long-term productivity of fractured gas reservoirs is directly controlled by the matrix flow and due to the low permeability of these reservoirs the flow velocity within the matrix tends to be very low
- 3. Gas flow behaviour for O₂, CO₂ and Air was analysed, and the results obeyed the criteria that governs low permeability unconventional reservoirs by dividing the flow stages into Darcy (linear) and Non-Darcy (radial) flow.
- 4. The Darcy region was investigated to establish the absolute permeability and how fluid viscosity affects the rate of flow. The results indicates that gases with higher viscosity tends to have lower flow rate. Confirming Darcy's equation that permeability of a porous medium is inversely proportional to the viscosity of the fluid.

