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1 **The degradation of microcystin-LR using doped visible light**
2 **absorbing photocatalysts.**

3

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11

12 **Keywords:** Visible photocatalyst, cyanotoxin, microcystin, water
13 treatment

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25 **Abstract**

26 Microcystins are one of the primary hepatotoxic cyanotoxins
27 released from cyanobacteria. The presence of these compounds in
28 water has resulted in the death of both humans and domestic and
29 wild animals. Although microcystins are chemically stable titanium
30 dioxide photocatalysis has proven to be an effective process for the
31 removal of these compounds in water. One problem with this
32 process is that it requires UV light and therefore in order to develop
33 effective commercial reactor units that could be powered by solar
34 light it is necessary to utilize a photocatalyst that is active with
35 visible light. In this paper we report on the application of four visible
36 light absorbing photocatalysts for the destruction of microcystin-LR
37 in water. The rhodium doped material proved to be the most
38 effective material followed by a carbon modified titania. The
39 commercially available materials were both relatively poor
40 photocatalysts under visible radiation while the platinum doped
41 catalyst also displayed a limited activity for toxin destruction.

42

43 **1. Introduction**

44 Cyanobacterial toxins produced and released by cyanobacteria
45 in freshwater around the world are well documented (Carmichael,
46 1995; Sivonen, 1996). Microcystins are the most common of the
47 cyanobacterial toxins found in water, as well as being the ones most
48 often responsible for poisoning animals and humans who come into
49 contact with toxic blooms and contaminated water (Codd et al.,
50 1989; Dunn, 1996; Yu, 1994; Tsuji et al., 1995). The most
51 important toxin is microcystin-LR which is a cyclic heptapeptide
52 containing the amino acid 3-amino-9-methoxy-2,6,8-trimethyl-10-
53 phenyldeca-4,6-dienoic acid (adda), with leucine and arginine in the
54 variable positions. Microcystins are chemically very stable and
55 conventional water treatment processes have so far proved
56 relatively ineffective in removing them (Keijola et al., 1988, Lahti et
57 al., 1989, Lawton and Robertson, 1999). The formation of
58 chlorinated by-products of the microcystins has been reported by
59 Merel et al. (2009). This group reported a detailed study of the use
60 of chlorination as a treatment process for the removal of
61 microcystins from water. Chlorination, this is only effective at
62 relatively high doses with a sufficient contact time. Although
63 chlorinated by-products have been characterised as yet the toxicity
64 of these by-products is unknown. The biodegradation of
65 microcystins -LR, -LF and the pentapeptide toxin nodularin in water
66 has previously been studied (Edwards et al., 2008; Torunska et al.,

67 2008) who reported degradation half lives for the toxins of between
68 4 and 18 d. Moreover the use of methods such as granular carbon
69 filtration and photochemical degradation have shown only limited
70 efficacy (Kaya and Sano, 1998, Reynolds, 1987; Tsuji et al., 1994).
71 Consequently there is a growing need for effective treatment
72 technologies for removal of microcystins from water.

73

74 We have previously reported the effectiveness of TiO_2
75 photocatalysis for the removal of microcystins in water (Robertson
76 et al., 1997; Robertson et al., 1998; Lawton and Robertson, 1999;
77 Robertson et al., 1999; Lawton et al., 1999; Cornish et al., 2000,
78 Liu et al., 2002; Liu et al., 2003). Although the process has been
79 demonstrated to be extremely effective in removing the toxin a
80 limitation of the process was the fact that the catalyst requires UV
81 light. If a suitable visible light absorbing photocatalyst could be
82 prepared the viability of the photocatalytic process would be
83 significantly improved as there could even be the potential of
84 operating the process using sun light. Choi et al. (2007) reported
85 the use of a nitrogen doped TiO_2 catalyst for the destruction of
86 microcystin under visible irradiation. Using this catalyst
87 approximately 50% of a 5 μM solution of microcystin-LR was
88 degraded in 30 min with virtually complete destruction being
89 achieved in 2 h. Pelaez et al. (2009) studied the photocatalytic
90 destruction of microcystin-LR using visible light absorbing N-F-

91 codoped TiO₂ nanoparticles. At pH 3 the toxin was completely
92 degraded within 300 min when irradiated with light at 420 nm. It
93 was proposed that under these conditions the electrostatic
94 interaction between the toxin and photocatalyst favoured the
95 decomposition process. The purpose of the research detailed in this
96 paper was to look at the potential effectiveness of a number of
97 visible absorbing photocatalysts for the destruction of microcystin-
98 LR. The efficiency of these materials was also compared to the
99 material that has been the subject of our previous work on
100 photocatalytic destruction of microcystin, the UV light absorbing
101 Degussa P25 TiO₂.

102

103 **2. Materials and experimental methods**

104 *2.1. Materials*

105 The two unmodified titania samples P25 (Degussa) and TH
106 (Titanhydrat, Kerr-McGee) were commercially available, whereas
107 the modified samples TiO₂-C (TiO₂-C1b: Sakthivel and Kisch, 2003),
108 $\{[\text{Ti}]\text{OPtCl}_4\text{L}\}^{n-}$, L = H₂O, OH⁻, n = 1, 2, (abbreviated as TiO₂-
109 Pt(IV)) (Burgeth and Kisch, 2002), and $\{[\text{TiO}_2]\text{-O-RhCl}_3(\text{H}_2\text{O})_2\}^-$
110 (abbreviated as TiO₂-Rh(III)) (5% RhCl₃/TH: Dai et al., 2008) were
111 prepared according to the literature. P25 TiO₂ was used as a
112 standard material for comparison on the relative effectiveness of
113 the catalysts detailed above. This has previously been established
114 as the most effective UV photocatalyst for the destruction of

115 cyanotoxins (Liu et al., 2009). Microcystin-LR was prepared as
116 previously reported (Edwards et al., 1996). The toxin was
117 resuspended in water prior to use.

118

119 *2.2 Photocatalysis*

120 The photocatalysis experiments were performed in 20 mL glass
121 vials under constant stirring at a distance of 30 cm from the front of
122 the light source (500 W Halogen, irradiation $393 \mu\text{M}^{-1}$, Temp 306 K
123), as illustrated in Fig. 1. A 2% w/v sodium nitrite filter was used to
124 eliminate and UV photons generated by the halogen source entering
125 the reaction vessel. An IR filter was also used to minimise any
126 thermal effects on the process. 50 mg of the photocatalysts were
127 added to 5 mL of a 0.1 mg mL^{-1} microcystin-LR solution. The
128 photocatalysis was conducted in Milli-Q water ($18.2 \text{ m } \Omega \text{ cm}$) and
129 the reaction pH was 4. After mixing for 5 min an initial sample was
130 removed to determine extent of dark adsorption. From previous
131 work it has been established that the dark adsorption process of
132 microcystins on titania photocatalysts is rapid and equilibrium is
133 established within the first five min (Robertson et al., 1997; Lawton
134 et al., 2003). The photocatalysis was then initiated and samples
135 were removed at 10 min intervals for the first 60 min after which
136 sampling was performed every 20 min to a maximum photocatalysis
137 period of 120 min.

138

139 *2.3 Analysis*

140 Treated samples were analysed by HPLC with photodiode array
141 detection as previously detailed (Lawton et al., 1994).

142

143 **3. Results and discussion**

144 In order to ensure that the visible activity of the photocatalysts
145 was being observed and there was no contribution to the process
146 from UV light, the process was initially examined using a standard
147 Degussa P25 material. On irradiating the suspension of P25 TiO₂
148 and microcystin with the halogen light filtered through 2% sodium
149 nitrite filter, no significant level of toxin degradation was observed
150 up to 120 min photocatalysis (Fig. 2a). The results of this initial
151 study confirmed that all residual UV light generated by the tungsten
152 halogen source had been removed, so only visible photons were
153 entering the reactor cell. Prior to using this filter set up a modest
154 destruction of microcystin-LR was achieved with unmodified
155 photocatalyst materials from the residual UV in the halogen source.
156 In order to determine the true level of visible activity of the
157 modified photocatalyst material, it was therefore necessary to utilise
158 this effective UV filter in order to eliminate any potential UV
159 activation of the materials.

160

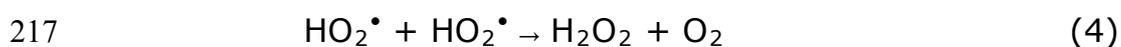
161 The photocatalytic activity of the five catalysts for the
162 destruction of microcystin-LR was subsequently assessed in the

163 same experimental setup. On adding the photocatalyst to the
164 microcystin solution it was initially clear that each of the materials
165 displayed varying levels of initial dark adsorption of the toxin. This
166 dark adsorption of the toxins on TiO₂ photocatalysts has been
167 previously reported and is believed to be due to a combination of
168 the surface charge of the photocatalysts material and the
169 hydrophobicity of the toxin (Lawton et al., 2003). Table 1
170 summarises for each of the photocatalysts the amount of
171 microcystin remaining in solution after dark adsorption and after 60
172 min of irradiation time. The photocatalytic destruction of the
173 microcystin over 120 min irradiation time for both modified and
174 unmodified materials under visible light irradiation is detailed in Fig.
175 2b. At the high photocatalyst concentration employed (10 g L⁻¹) the
176 amount of absorbed light should be about the same in each
177 experiment and reaction rates are therefore comparable. Unlike the
178 two unmodified titania samples, which do not absorb visible light, all
179 modified photocatalysts efficiently decomposed the toxin, with TiO₂-
180 C and TiO₂-Rh(III) having the highest activity. In the latter system
181 half of the toxin present in solution was degraded after 10 min
182 whereas TiO₂-C needed 30 min to induce the same amount of
183 destruction. As can be recognized, only the TiO₂-Rh(III) sample
184 enabled complete toxin degradation after 60 min.
185

186 Scheme 1 summarizes the positions of band edge and
187 absorption onset of the various photocatalysts. It is rather unlikely
188 that the small changes in the redox potentials of the light-generated
189 electron and holes are responsible for the different degradation
190 activities. It is more likely that the different chemical nature of the
191 reactive holes seems to be decisive. It was proposed that in the
192 case of the Rh(III) modified material the hole is a Rh(IV) species
193 (Eq. 1, Dai et al., 2008), whereas in TiO₂-C and related carbon-
194 modified titania it may be a radical or radical cation of a condensed
195 aromatic compound (Neumann et al., 2005; Zabek et al., 2009 and
196 references cited therein). It appears very probable that such
197 different species oxidize microcystin with different reaction rates. It
198 is known that the interfacial electron transfer from the conduction
199 band to oxygen (Eq. 2) is the rate-determining step of most
200 semiconductor catalyzed photooxidation reactions (Gerischer and
201 Heller, 1991; Schwitzgebel et al., 1995). If this would be the case,
202 then TiO₂-C should react faster than TiO₂-Rh(III) since the driving
203 force is lower for the latter due to the corresponding flatband
204 positions of -0.48 V (Sakthivel and Kisch, 2003) and -0.34 V (Dai
205 et al., 2008) for the carbon- and rhodium-modified material,
206 respectively. However, it cannot be excluded that charge
207 generation in TiO₂-Rh(III) is more efficient resulting in a higher
208 electron concentration and therefore in faster oxygen reduction (Eq.
209 2). As a result of this also the concentration of the hydroxyl radical,

210 the other strongly oxidizing intermediate generated through
211 reaction steps according to Eq. 3-6, are expected to be higher than
212 in TiO₂-C.

213



220

221 The observation that TiO₂-Pt(IV) is much less active than the
222 rhodium and carbon modified samples suggests that the adsorbed
223 chlorine radical (representing the reactive hole) generated through
224 a homolytic Pt-Cl bond cleavage (Burgeth and Kisch, 2002) can
225 induce only an inefficient microcystin oxidation. TiO₂-Pt(IV) exhibits
226 the strongest dark adsorption of 84%. A light-induced desorption of
227 microcystin may be responsible for the small concentration increase
228 found for P25.

229

230 In the work performed by Choi et al. (2007) using a nitrogen
231 doped titania sample 50% toxin destruction was achieved in around
232 30 min with complete decomposition reported within 2 h visible light
233 photocatalysis. It is not possible to directly compare the results of

234 this study with those obtained in the work of Choi et al. (2007) as
235 the experimental conditions such as the initial toxin concentration
236 and light intensity were not the same.

237

238 In order to assess the relative efficiency of the visible light
239 photocatalytic process to the UV absorbing titania, the degradation
240 of microcystin-LR was examined using both a standard Degussa P25
241 material and a modified P25 catalyst $\text{TiO}_2\text{-Pt(IV)}$ under UV
242 irradiation. For both materials the microcystin was decomposed
243 within 10 min of photocatalysis (Fig. 2c) as compared to about 20
244 min for the best visible light photocatalyst $\text{TiO}_2\text{-Rh(III)}$. This
245 unexpected result can be rationalized by assuming that holes
246 generated below the valence band edge ("hot carriers") rather
247 oxidize microcystin than relax to the conduction band edge level.
248 The opposite behaviour may be responsible for the lower activity of
249 $\text{TiO}_2\text{-Rh(III)}$.

250

251 The use of artificial UV light sources for photocatalytic water
252 treatment represents one of the most significant costs of the
253 process. Consequently there has been significant interest in utilizing
254 sunlight as the energy source for large scale photocatalytic water
255 treatment (Bahnemann, 2004). Unfortunately UV light represents
256 approximately 5% of the energy in solar light, while 45% is in the
257 visible region. Therefore at the planet's surface, the typical UV-flux

258 of 20 to 30 W m⁻², the sun generates 0.2 to 0.3 mol photons m⁻² h⁻¹
259 between 300-400 nm for potential utilisation by photocatalytic
260 reactors (Bahnemann, 1994). If visible light absorbing catalysts
261 were to be utilised potentially up to nine times this energy could be
262 available, depending on the band gap of the catalyst being utilized.
263 Consequently, although it would appear in this study that the
264 TiO₂/UV process is more efficient than the TiO₂/Visible process, the
265 advantages of being able to utilise visible light far outweigh the
266 relatively poorer photocatalytic efficiency particularly for any large
267 scale application. There may be potential toxicity risks associated
268 with using metal doped titania materials. This risk would depend on
269 the potential leaching of the dopant metals from the titania material
270 into the water. In any commercial application it would be necessary
271 to assess the risk of such a leaching process occurring and this
272 would need to be a subject of more in depth future work.

273

274 **4. Conclusions**

275 The photocatalytic degradation of the cyanotoxin, microcystin-
276 LR has been achieved using visible light absorbing photocatalysts.
277 The process was demonstrated to be particularly efficient for the
278 TiO₂-Rh(III) material with 90% of the toxin being destroyed in 20
279 min irradiation. Although the TiO₂/UV process was still relatively
280 more efficient, the advantages of being able to use visible light to
281 drive this process significantly outweigh the marginally faster

282 kinetics under UV irradiation. These visible light absorbing materials
283 could therefore significantly improve the viability of semiconductor
284 photocatalysis as a practical water treatment process for removal of
285 microcystins from potable water supplies.

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411

412 **List of Captions for Figures.**

413

414 **Fig. 1.** Experimental set up for Photocatalysis Studies.

415

416 **Fig. 2.** a) Degradation of microcystin-LR in the presence of P25
417 with no illumination. b) Degradation of microcystin-LR using
418 different photocatalyst materials. TH ▲, P25 ■, TiO₂-C ◆, TiO₂-
419 Pt(IV)◻ and TiO₂-Rh(III)◊. c) Degradation of microcystin-LR in the
420 presence of modified P25 TiO₂-Pt(IV) ■ and P25 ◆ under UV
421 illumination using a deuterium light source.

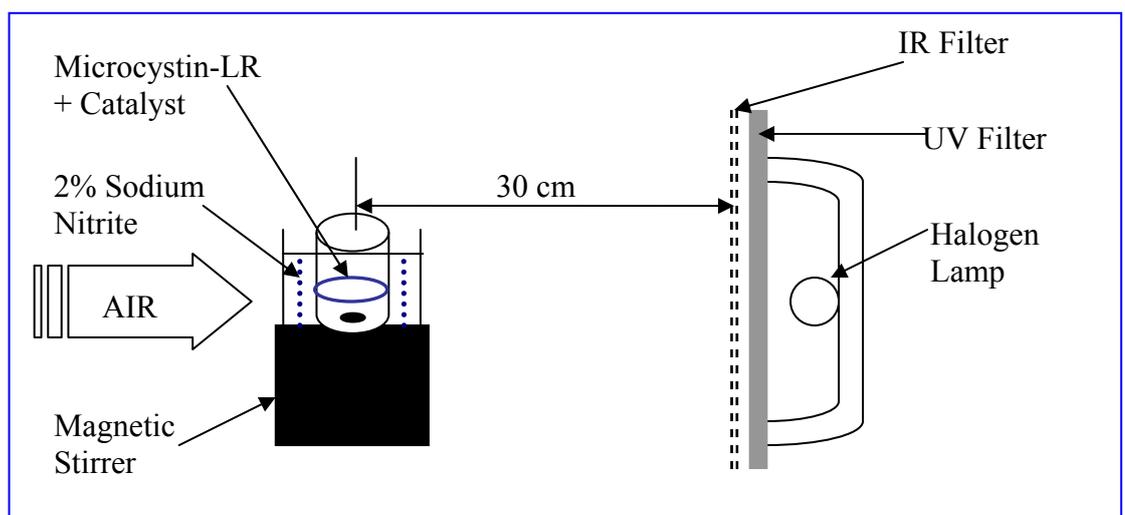
422

423 **Scheme 1.** Band edge positions and onset of absorption (---)
424 of various photocatalysts. Lengths of arrows correspond to energy
425 of exciting light ($\lambda \geq 400$ nm). (Sakthivel and Kisch, 2003; Burgeth
426 and Kisch, 2002; Dai et al., 2008.)

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Fig. 1

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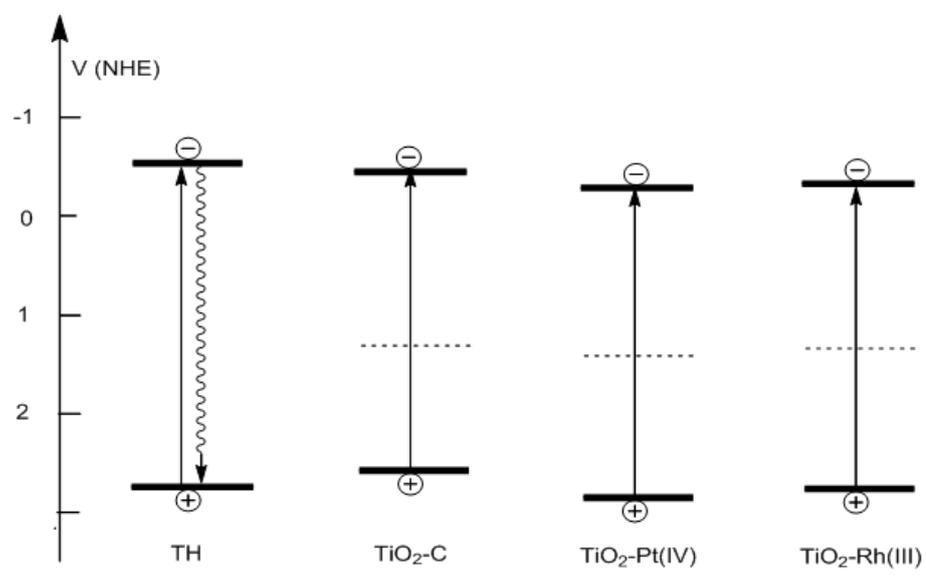
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447 **Table 1.** Percentage of Microcystin-LR in solution after
 448 equilibration in the dark (a) and after 60 min of visible light
 449 irradiation (b).
 450

Photocatalyst	% Microcystin-LR remaining in solution	
	t = 0	T = 60 min
P25	57	60
TH	80	70
TiO ₂ -Pt(IV)	16	10
TiO ₂ -C	68	20
TiO ₂ -Rh(III)	40	0

451

452
453



Scheme 1.

454
455